

Amendments to the Claims

1. (Currently Amended) A process to prepare a haze free base oil having a kinematic viscosity at 100 °C of greater than 10 cSt from a Fischer-Tropsch wax feed comprising the following steps:
 - (a) reducing the wax content of a Fischer-Tropsch wax feed by contacting the feed with a hydroisomerisation catalyst under hydroisomerisation conditions at a remote location to form an intermediate product having a wax content between 10 and 35 wt%;
 - (b) transporting the intermediate product having the reduced wax content as obtained in step (a) from the remote location to another location closer to the end-user; and
 - (c) solvent dewaxing the transported intermediate product to obtain a haze free base oil at the location closer to the end-user.
2. (Previously Presented) The process according to claim 1, wherein the feed to step (a) has a 10 wt% recovery boiling point of above 500 °C and a wax content of greater than 50 wt%.
3. (Previously Presented) The process according to claim 2, wherein the wax content in the feed is between 60 and 95 wt%.
4. (Previously Presented) The process according to claim 2, wherein the 10 wt% recovery boiling point of the feed is between 500 and 550 °C.

Claim 5 (Canceled).

6. (Previously Presented) The process according to claim 1, wherein the intermediate product has a congealing point of between 20 and 60 °C.
7. (Previously Presented) The process according to claim 1, wherein more than 50 wt% of the intermediate product boils above the 10 wt% recovery point of the feed used in step (a).

8. (Previously Presented) The process according to claim 7, wherein more than 70 wt% of the intermediate product boils above the 10 wt% recovery point of the feed used in step (a).
9. (Previously Presented) The process according to claim 1, wherein the hydroisomerisation catalyst used in step (a) is a substantially amorphous based catalyst comprising a silica-alumina carrier and a noble or non-noble Group VIII metal.
10. (Previously Presented) The process according to claim 1, wherein the hydroisomerisation catalyst used in step (a) is a molecular sieve based catalyst and a noble or non-noble Group VIII metal.
11. (Previously Presented) The process according to claim 1, wherein step (b) is performed by means of a ship and wherein containers on the ship are first purged with nitrogen before loading and wherein the nitrogen is obtained in an air-separation unit which unit also isolates oxygen for use to make syngas which in turn is used as feedstock to prepare the Fischer-Tropsch wax feed.
12. (Currently Amended) A process to prepare a lubricant composition not containing a viscosity modifier additive by blending a low viscosity base oil with a haze free base oil having a kinematic viscosity at 100°C of greater than 10 cSt from a Fischer-Tropsch wax feed prepared by a process comprising the following steps:
- (a) reducing the wax content of a Fischer-Tropsch wax feed by contacting the feed with a hydroisomerisation catalyst under hydroisomerisation conditions at a remote location to form an intermediate product having a wax content between 10 and 35 wt%;
 - (b) transporting the intermediate product having the reduced wax content as obtained in step (a) from the remote location to another location closer to the end-user; and
 - (c) solvent dewaxing the transported intermediate product to obtain a haze free base oil at the location closer to the end-user.
13. (Previously Presented) The process according to claim 12, wherein the feed to step (a) has a 10 wt% recovery boiling point of above 500 °C and a wax content of greater than 50 wt%.

14. (Previously Presented) The process according to claim 12, wherein the wax content in the feed is between 60 and 95 wt%.

15. (Previously Presented) The process according to claim 12, wherein the 10 wt% recovery boiling point of the feed is between 500 and 550 °C.

Claim 16 (Canceled).

17. (Previously Presented) The process according to claim 12, wherein the intermediate product has a congealing point of between 20 and 60 °C.

18. (Previously Presented) The process according to claim 12, wherein more than 50 wt% of the intermediate product boils above the 10 wt% recovery point of the feed used in step (a).

19. (Previously Presented) The process according to claim 12, wherein more than 70 wt% of the intermediate product boils above the 10 wt% recovery point of the feed used in step (a).

20. (Previously Presented) The process according to claim 12, wherein the hydroisomerisation catalyst used in step (a) is a substantially amorphous based catalyst comprising a silica-alumina carrier and a noble or non-noble Group VIII metal.

21. (Previously Presented) The process according to claim 12, wherein the hydroisomerisation catalyst used in step (a) is a molecular sieve based catalyst and a noble or non-noble Group VIII metal.

22. (Previously Presented) The process according to claim 12, wherein step (b) is performed by means of a ship and wherein containers on the ship are first purged with nitrogen before loading and wherein the nitrogen is obtained in an air-separation unit which unit also isolates oxygen for use to make syngas which in turn is used as feedstock to prepare the Fischer-Tropsch wax feed.